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1. A viscous fluid (specific gravity, $SG = 1.26$; kinematic viscosity, $\nu = 1.28 \times 10^{-2} \text{ ft}^2/\text{s}$) is contained between two large, horizontal parallel plates as shown in Fig. 1. The fluid moves between the plates under the action of a pressure gradient B . When the lower plate is pulled with a velocity V while the upper plate is fixed, the velocity distribution for this flow takes the form

$$u(y) = \frac{B}{2\mu}(y^2 - hy) + V\left(1 - \frac{y}{h}\right)$$

For $V = 0.02 \text{ ft/s}$, $h = 1.0 \text{ in.}$, $B = -0.334 \text{ lb/ft}^3$, and the plate area $A = 100 \text{ ft}^2$, determine (a) the shearing stress τ acting on the moving plate and (b) the required force $F = \tau \cdot A$ and (c) power $P = F \cdot V$ to pull the plate. (Note: $\nu = \mu/\rho$ and use $\rho_{\text{water}} = 1.94 \text{ slugs/ft}^3$)

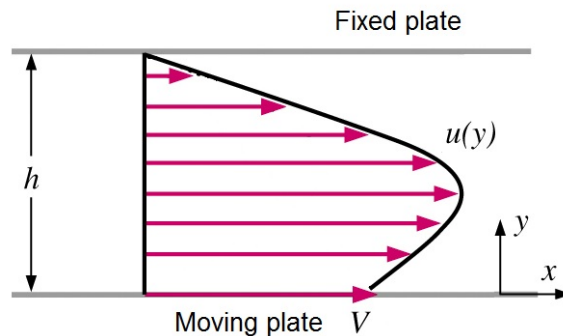


Figure 1

2. The 0.5-m-radius half-cylinder barrier in Fig. 2 is 8 m long into the paper and rests in static equilibrium against a wall. The contact between cylinder and wall is frictionless. Find (a) the horizontal force (magnitude F_H and location y_{cp}) and (b) vertical force (magnitude F_V) exerted on the curved surface of the barrier and (c) the barrier weight W . You can use geometric properties shown on Figure 3. (Note: $\gamma = 9.80 \text{ kN/m}^3$)

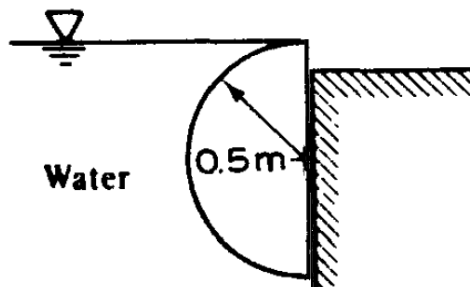
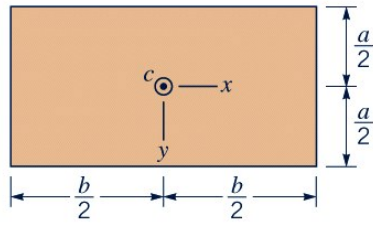


Figure 2

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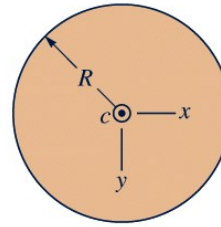
$$A = ba$$

$$I_{xc} = \frac{1}{12} ba^3$$

$$I_{yc} = \frac{1}{12} ab^3$$

$$I_{xyc} = 0$$

(a) Rectangle

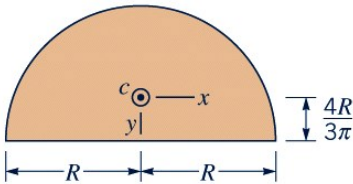


$$A = \pi R^2$$

$$I_{xc} = I_{yc} = \frac{\pi R^4}{4}$$

$$I_{xyc} = 0$$

(b) Circle



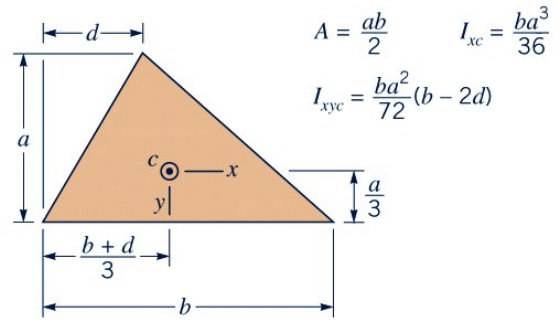
$$A = \frac{\pi R^2}{2}$$

$$I_{xc} = 0.1098R^4$$

$$I_{yc} = 0.3927R^4$$

$$I_{xyc} = 0$$

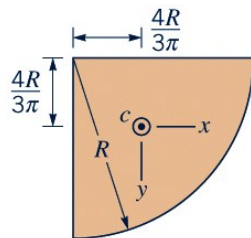
(c) Semicircle



$$A = \frac{ab}{2} \quad I_{xc} = \frac{ba^3}{36}$$

$$I_{xyc} = \frac{ba^2}{72}(b - 2d)$$

(d) Triangle



$$A = \frac{\pi R^2}{4}$$

$$I_{xc} = I_{yc} = 0.05488R^4$$

$$I_{xyc} = -0.01647R^4$$

(e) Quarter circle

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Figure 3: Geometric Properties of some common shapes

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3. Water ($\gamma = 62.4 \text{ lb/ft}^3$) flows steadily from a large tank as shown in Fig. 4. The deflection in the mercury manometer is 1 in. and viscous effects are negligible. Determine (a) the volume flow rate Q and (b) the water-jet velocity V_j leaving the 3-in. diameter nozzle exit. (Note: $SG = 13.56$ for mercury and $g = 32.2 \text{ ft/s}^2$)

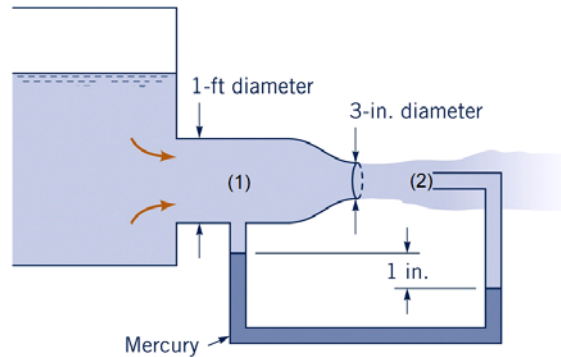


Figure 4

4. According to potential theory for the flow approaching a rounded two-dimensional body, as in Fig. 5, the velocity approaching the stagnation point is given by $\underline{V} = U(1 - a^2/x^2)\hat{i}$, where a is the nose radius and U is the velocity at far-upstream. If the fluid is SAE 30 oil ($\rho = 917 \text{ kg/m}^3$) with $U = 2 \text{ m/s}$ and $a = 6 \text{ cm}$, calculate (a) the fluid velocity u , (b) the acceleration a_x , and (c) the pressure gradient dp/dx at point 1 (i.e., at $x = -2a$). For part (c), use the Euler equation, $\rho a_x = -dp/dx$.

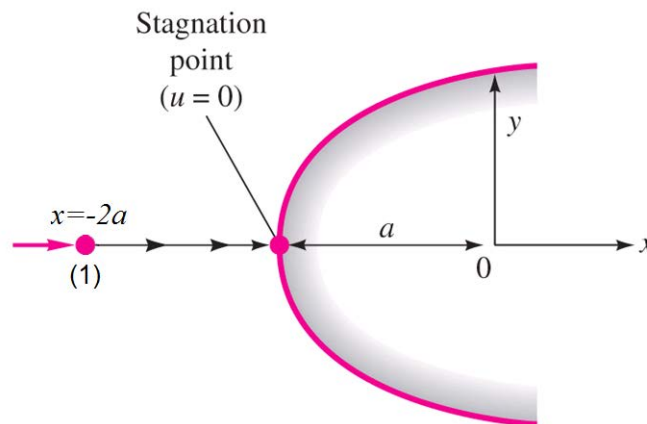


Figure 5